

Adsorption of Nickel and Copper from Water by Waste Nitrification Organisms

*Sukru Aslan and Ugur Savas Topcu Faculty of Engineering, Department of Environmental Engineering, Cumhuriyet University, Turkey

Abstract:

The heavy metals; nickel and copper biosorption performance of waste nitrifying sludge was determined at various temperatures and pHs. It was found that the organic content and NH_4 -N concentrations in the water increases with increasing the temperature. The sorption of heavy metals also increased with increasing the temperatures. The rise of adsorption with temperature may enlarge the pore size to some extent which may also affect the adsorption capacity of biosludges. The highest sorption capacity of bioslude was determined at the pH of 5.0. The data obtained from the experiments showed that the contact time of about 360 min and 1440 min were sufficient to achieve equilibrium time for nickel and copper, respectively.

Key words: Biosorption, copper, nickel, waste sludge

1. Introduction

Heavy metal contamination of the environment is a severe public health problem. An important source of water pollutants is industrial discharge wastewater which contains heavy metals. Most industrial wastewaters are discharged into the water body without proper management process. High concentrations of heavy metal affect negatively human, animal and vegetation in the water body. Because of unique characteristics of heavy metals, which are non-biodegradable and accumulated by living organisms, are the main environmental concerns [1].

Treatment of the wastewater including heavy metal ions became particularly difficult due to implementation of more restrict law regulations that control the concentration of pollutants in effluents discharged into waters and soil on the level lower than 1 mg/kg [2]. The treatment processes - such as such as ion exchange, chemical precipitation and coagulation- flocculation, membranes processes - for the removal of low concentrations of metal ions are often considered as an ineffective and/or very expensive method to achieve target level. Technical limitations, economical constraints, and environmental criteria are some issues that explain the need for alternative treatment processes for the removal of heavy metal in wastewater [3].

In last two decades, biosorption has been widely investigated for the removal of heavy metal. Microorganisms are found to be capable of efficiently accumulating heavy-metal ions. Among the numerous natural materials for removing heavy metals, biosorbents such as bacteria, fungi,

^{*}Corresponding author: Address: Faculty of Engineering, Department of Environmental Engineering, Cumhuriyet University, 58140, Sivas TURKEY. E-mail address: saslan@cumhuriyet.edu.tr, Phone: +903462191010 Fax: +903462191177

and algae [4-7], yeast [8-10], waste tea [11, 12], bael tree leaf powder [13], sugarcane bagasse pith [14], *chlorella vulgaris* [8], eggshell [1,15] have attracted attention as a low-cost sorbents from wastewater. Adsorption potential of the waste biosolids is summarized in Table 1.

Biosorbents	$q_m (mgNi^{2+}/g)$	$q_m (mgCu^{2+}/g)$	References
Clarified sludge	14.3		[16]
Spirulina platensis	69.04		[17]
Acid-treated alga	44.247		[18]
Untreated alga	40.983		[18]
Green alga Spirogyra		133.3	[4]
Dried activated sludge		62.50	[19]
P. chrysosporium		248.15	[20]
Bacillus subtilis		146.09	[21]
Powdered waste activated sludge		117	[22]
Activated sludge		7.94	[23]
Ochrobactrum anthropi		32.6	[24]

Table 1. Comparison of maximum monolayer adsorption on Ni (II) and Cu (II) ions onto various adsorbents

In recent years, water pollutants removal by biosorption using waste sludge which is produced in the biological treatment plants is widely used in the laboratory studies [26-32]. The use of dead cell, which is waste materials, as metal binding compounds has been gaining advantage because it is not affected from the heavy metals. As a consequence, activated sludge produced in the biological treatment facilities of the treatment plant is considered as a good bioadsorbent for the removal of heavy metal ions from industrial wastewater [26].

Biological nitrification is a widely applied process in the wastewater treatment facilities. Aerobic autotrophic bacteria are responsible for nitrification in the biological processes. In the nitrification process, NH_4^+ -N is first oxidized into NO₂-N by *nitrosomonas sp.* (ammonium oxidizing bacteria, AOB) and then NO₂-N is rapidly oxidized to NO₃-N by *nitrobacter sp.* (nitrite oxidizing bacteria, NOB). The overall stoichiometric equation of nitrification process can be written as [33];

 $NH_4 + 1.815 O_2 + 0.1304 CO_2 \longrightarrow 0.0261C_5H_7O_2N + 0.973 NO_3^- + 0.921 H_2O + 1.973 H^+$ (Equation 1) As can be seen from the equation, about 25% of the consumed NH_4^+ is converted to the biomass in the nitrification process and excess biomass is disposed from the wastewater treatment plants.

The purpose of this investigation was to study the biosorption of Cu^{2+} and Ni^{2+} from synthetic water using nitrifying sludge obtained from a laboratory scale reactor. In this study, effects of the temperature and pH on the COD release from the biomass was investigated.

2. Materials and Method

2.1. Enrichment of microorganisms

Nitrifying sludge was obtained from the laboratory scale bioreactor which was operated about 5 years. The inorganic medium contained (in mg/L): NH₄Cl (764.3), Na₂EDTA (4.83), CuSO₄ (0.0046), Thiamine (0.1), ZnSO₄.7H₂O (0.023), CoCl₂.6H₂O (0.0119), Na₂MoO₄.2H₂O (0.066), MgSO₄.7H₂O (36.97), NaHCO₃ (226), CaCl₂.2H₂O (36.74), H₃BO₃ (1.0), FeCl₃.6H₂O (0.316), K₂HPO₄ (1960), and KH₂PO₄ (1920).

2.2. Preparation of adsorbent

The biomass was washed several times with tap and pure water to remove impurities. Water was evaporated at 60°C on a water bath for about 48 h and the biomass was oven dried at 60°C for 24 h. The dried biomass was crushed and sieved into several fractions.

2.3. Sorption Studies

The synthetic solutions were prepared by diluting Ni^{2+} and Cu^{2+} standard stock solutions (250 mg/L) obtained by dissolving known masses of NiCl₂.6H₂O and CuCl₂ in the distilled water. A known amount of biomass (0,025 g) was used throughout the experiments. Final volumes of the solution was 100 mL. Experimental studies were carried in 250 mL glass-stoppered Erlenmeyer flasks. Batch experimental studies were performed in an orbital incubator shaker (Gerhardt) at a constant speed of 150 rpm. All solutions were prepared from analytical reagent chemicals. Fresh dilutions of the synthetic wastewater were used in the experiments.

Effects of temperature and pH on the sorption of heavy metals were tested at various levels. Initial pHs of the solutions were adjusted using H_2SO_4 or NaOH solutions. The batch units were agitated in an orbital incubator shaker for a contact time varied in the range 0–2880 min at various temperatures.

2.4. Analytical methods

In order to get supernatant liquids, the samples were centrifuged at 4000 rpm for 10 min (NF800, NUVE). Concentrations of Ni²⁺ and Cu²⁺ in the solutions were determined with a Merck photometer (PHARO100). A spectraquant analytical kits (Merck, 14785 and 14767) were used to measure Cu²⁺ and Ni²⁺ concentrations in the initial and final solutions. COD concentrations of the influent and effluent samples were determined according to standard methods [34]. Concentrations of NH₄-N in the clear sample was determined with Merck photometer (PHARO 100) using analytical kits; NH₄-N (14752). The analysis of samples was carried out at the ambient temperature.

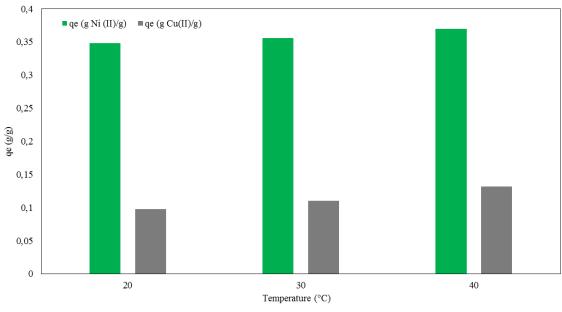
3. Results and Discussion

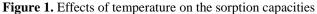
The data obtained from the experiments showed that the contact time of about 360 min and 1440 min were sufficient to achieve equilibrium time for nickel and copper, respectively.

3.1. Effect of temperature

It was found that the concentrations of COD and NH₄-N in the water and sorption capacities of biosolids increased with increasing temperature (Figure 1 and 2). Cu^{2+} and Ni²⁺ ions uptake capacity of biosolids increased with increasing temperature up to 40 0 C. At a temperature of about 20 0 C, the removal efficiency of Cu²⁺ and Ni²⁺ at equilibrium was 88 % and 24%, respectively. The highest removal efficiencies (95 % for Cu (II) and 33% for Ni (II)) was achieved at the temperature of 40 0 C.

Elevating the temperature from 20 to 40 0 C, the release of organic contents into the aqueous solution increased from 6 to 11 mg COD/L. The value of q_e elevated from 0.098 to 0.132 g Ni(II)/g biosolids and from 0.348 to 0.37 g Cu (II)/g biosolids by increasing temperature from 20 to 40 0 C. Results might be attributed to the creation of some new active sites on the biosolids and increase in collision frequency between adsorbent and heavy metal ions at high temperatures. In addition to that, the rise of adsorption with temperature may enlarge the pore size to some extent which may also affect the adsorption capacity [35].





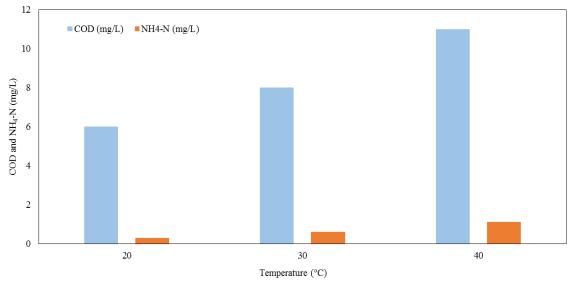


Figure 2. Temperature effects on the COD and NH₄-N concentrations

3.2. Heavy metal sorption at different initial pH

The acidity of solution is an important parameter for the sorption of heavy metals from aqueous solutions since the value of pH is responsible for protonation of metal binding sites, Ni^{2+} and Cu^{2+} speciation in the solution [2]. The uptake of heavy metals was investigated as the function of pH value of 3.0, 4.0 and 5.0.

Sorption of Ni^{2+} and Cu^{2+} after interaction of heavy metals and biosolids sorbent is presented in Figure 3. Heavy metal uptake by biosolids was a function of initial solution pH. The lowest

adsorption efficiency of 15% and 69% were observed at the pH value of 3.0 for Ni^{2+} and Cu^{2+} , respectively. Increasing the pH value of 5.0, sorption capacities (q_e) increased significantly to 0.122 g Ni(II)/g and 0.378 g Cu (II)/g. The ionization degree of heavy metal and the surface property of the biosolids may be affected by the pH. The concentration of COD and NH₄-N was significantly elevated at low pH (Figure 4).

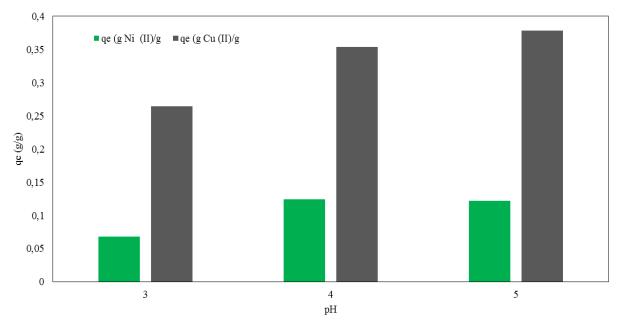


Figure 3. Effects of pH on the sorption capacities

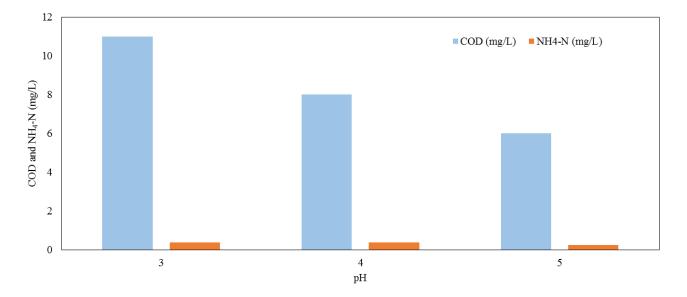


Figure 4. Effects of pH on the COD and NH₄-N concentrations

Conclusion

The possibility of use of waste dried nitrifying sludge to remove Cu (II) and Ni (II) ions from aqueous solution was investigated. Results indicating that the waste biosolids might be used for heavy metal removal from aqueous solution. The maximum sorption capacities were determined at the pH value of 5.0. Adsorption of Cu^{2+} and Ni^{2+} was highly temperature dependent. It was found that the organic content was increases with increasing the temperature. The sorption of heavy metals also increased with increasing the temperatures.

Acknowledgment: This study was supported by The Research Fund of Cumhuriyet University (CUBAP) under Grant No. M-539, Sivas, Turkey.

References

[1] Ghazy, S El-S. El-Asmy A A H, El-Nokrashy A M. Batch removal of nickel by eggshell as a low cost sorbent. Int J Ind Chem 2011; 2;4;242-252.

[2] Chojnacka K. Biosorption of Cr (III) ions by eggshells. J Hazard Mater 2005; B121; 167–173.

[3] Bermúdez Y G, Rico ILR, Bermúdez O G, Guibal E. Nickel biosorption using *Gracilaria* caudata and *Sargassum muticum*. Chem Eng JI 2011;166;122–131.

[4] Gupta VK, Rastogi A, Saini VK, Jain N. Biosorption of copper(II) from aqueous solutions by Spirogyra species. J Colloid Interface Sci 2006;296;59–63.

[5] Kapoor A, Viraraghavan T. Heavy metal biosorption sites in *Aspergillus niger*. Bioresource Technol 1997; 61:221–7.

[6] Rao PR, Bhargavi Ch, Studies on Biosorption of heavy metals using pretreated biomass of fungal species. Int J Chem Chem Eng 2013;3;3;171-180.

[7] Yeddou N, Bensmaili A. Equilibrium and kinetic modelling of iron adsorption by eggshells in a batch system: effect of temperature. Desalination 2007;206; 127-134.

[8] Aksu Z, Donmez G. Comparison of copper (II) biosorptive properties of live and treated *Candida sp.* J Environ Sci Heal A 2001;A36;3; 367–381.

[9] Cojocaru C, Diaconu M, Cretescu I, Savi J, Vasi V. Biosorption of copper (II) ions from aqua solutions using dried yeast biomass. Colloid Surface A 2009; 335;181–188.

[10] Lokeshwari N, Joshi K. Biosorption of heavy metal (Chromium) using biomass. Global J Environ Res 2009;3; (1): 29-35.

[11] Malkoc E, Nuhoglu Y. Removal of Ni(II) ions from aqueous solutions using waste of tea factory: Adsorption on a fixed-bed column. J Hazard Mater 2009;B135;328–336.

[12] Shah J., Jan M R., Haq A., Zeeshan M. Equilibrium, kinetic and thermodynamic studies for sorption of Ni (II) from aqueous solution using formaldehyde treated waste tea leaves. J Saudi Chem Soc 2012; doi:10.1016/j.jscs.2012.04.004

[13] Kumar PS, Kirthika K. Equilibrium and kinetic study of adsorption on nickel from aqueous solution onto bael tree leaf powder. J Eng Sci Techno 2009;4; 4;351 – 363.

[14] Krishnan K A, Sreejalekshmi KG, Baiju RS. Nickel(II) adsorption onto biomass based activated carbon obtained from sugarcane bagasse pith. Bioresource Techno 2011;102;10239–10247.

[15] Polat and Aslan, Polat, A.; Aslan, S. Kinetic and isotherm study of cupper adsorption from aqueous solution using waste eggshell. J Environ Eng Landsc 2014;22;02;132-140.

[16] Hannachi Y., Shapovalov N A., Hannachi A. Adsorption of nickel from aqueous solution by the use of low-cost adsorbents. Korean J Chem Eng 2010; 27(1), 152-158.

[17] Celekli A., Bozkurt H. 2011. Bio-sorption of cadmium and nickel ions using *Spirulina platensis*: Kinetic and equilibrium studies. Desalination 275; 141–147.

[18] Gupta V K., Rastogi A., Nayak A. 2010. Biosorption of nickel onto treated alga (*Oedogonium hatei*): Application of isotherm and kinetic models. J Colloid Interface Sci 342; 533–539.

[19] Benaïssa H, Elouchdi M.A. Biosorption of copper (II) ions from synthetic aqueous solutions by drying bed activated sludge. J Hazard Mater 2011; 194; 69–78.

[20] Sing C., Yu J. Copper adsorption and removal from water by living mycelium of white-rot fungus *Phanerochaete chrysosporium*. Water Res 1998;32;9;2746–2752.

[21] Volesky B., Holan Z.R. Review: Biosorption of heavy metals. Biotechnol Prog 1995;11;235–250.

[22] Pamukoglu MY, Kargi F. 2006. Removal of copper (II) ions from aqueous medium by biosorption onto powdered waste sludge. Process Biochem 41;1047–1054.

[23] Muraleedharan T.R., Tyengar L., Venkobachar C. Screening of tropical woodrotting mushrooms for copper biosorption, Appl. Environ. Microbiol 1995;61; 3507–3508.

[24] Ozdemir G., Ozturk T., Ceyhan N., Isler R., Cosar T., Heavy metal biosorption by biomass of Ochrobactrum anthropi producing exopolysaccharide in activated sludge. Bioresource Technol 2003;90; 71–74.

[26] Al-Qodah, Z., Biosorption of heavy metal ions from aqueous solutions by activated sludge. Desalination 2006;196;164–176.

[27] Chowdhury Md R I, Mulligan C N, Biosorption of arsenic from contaminated water by anaerobic biomass. J Hazard Mater 2011; 190; 486–492.

[28] Hammaini A, Gonzalez F, Ballester A, Blazquez M L, Munoz JA. Biosorption of heavy metals by activated sludge and their desorption characteristics. J Environ Manage 2007;84;419–426.

[29] Jianlong W, Yi Q, Horan N, Stentiford E, Bioadsorption of pentachlorophenol (PCP) from aqueous solution by activated sludge biomass. Bioresource Technol 2000; 75; 157±161.

[30] Liu D, Tao Y, Li K, Yu J. Influence of the presence of three typical surfactants on the adsorption of nickel (II) to aerobic activated sludge, Bioresource Techno 2012;126:56–63.

[31] Pagnanelli F, Mainelli S, Bornoroni L, Dionisi D, Toro L, Mechanisms of heavy-metal removal by activated sludge. Chemosphere 2009; 75;1028–1034.

[32] Remenarova L, Pipiska M, Hornik M, Rozloznik M, Jozef A, Lesny J. Biosorption of cadmium and zinc by activated sludge from single and binary solutions: Mechanism, equilibrium and experimental design study. J Taiwan Inst Chem E 2012;43;433–443.

[33] Rittmann B E., McCarty P L. Environmental Biotechnology: Principles and Applications, International Edition 2001, 754p.

[34] APHA, AWWA, WPCF Standard Methods for the Examination of water and wastewater, 19th ed., American Public Health Association/American Water Works Association/Water Environment Federation, Washington DC, USA, 1995.

[35] Demirbas E. Dizge E. Sulak, MT. Kobya M. Adsorption kinetics and equilibrium of copper from aqueous solutions using hazelnut shell activated carbon. Chem Eng J 2009; 148: 480–487.